

IRVING PAPER

IMPROVED EFFLUENT TREATMENT SYSTEM

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OBJECTIVE



The objective of this project is to upgrade the wastewater treatment system at the Irving Paper mill such that it exceeds newly proposed effluent regulations by Environment Canada.

PROBLEM DEFINITION

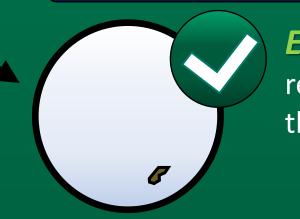
Untreated

Wastewater

Current Treatment System **Unable** to meet the 2021 regulations

Proposed Upgrade

Large Scraps



Exceeds quality required to meet the 2021 regulations

IRVING PAPER MILL

The Irving Paper mill is in the city of Saint John, New Brunswick, where a Thermomechanical Pulping process is used to produce supercalendered paper and newsprint. The yearly production of the facility's two paper machines amounts to 420,000 tonnes.



Air

Aerated

Stabilization

Sludge

Thickening

Water

Flocculant

Sludge

Increase from

1% to **5%**

Water

REGULATION CHANGES



In 2021, the Pulp and Paper Effluent Regulations are being modernized from their 1992 implementation. The aquatic discharge limits for various pollutants have been significantly reduced. Irving Paper Limited's (IPL) main concern is reducing the discharge of Total Suspended Solids (TSS) and Biochemical Oxygen Demand (BOD), nevertheless meeting the limits of other constituents.

ESTIMATED COSTS



Sludge

Dewatering

Sludge

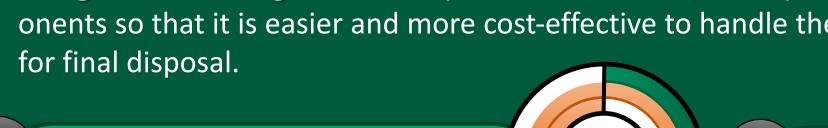
Total Capital Investment: *\$14.6M* Annual Operating Costs: **\$3.0M**

PROPOSED DESIGN

- **Packed Aeration** is the process of adding air into wastewater inside a biofilm reactor to allow aerobic bio-degradation of the pollutants.
- ▶ **Secondary Clarification** is used to settle the generated biomass from the treated effluent stream prior to discharge.
- ▶ *Sludge Thickening* is a process that decreases the sludge volume to reduce the footprint and power requirements for sludge dewatering.
- ▶ Sludge Dewatering further separates the solid and liquid components so that it is easier and more cost-effective to handle the sludge

Gain **72%** BOD

D: 40m

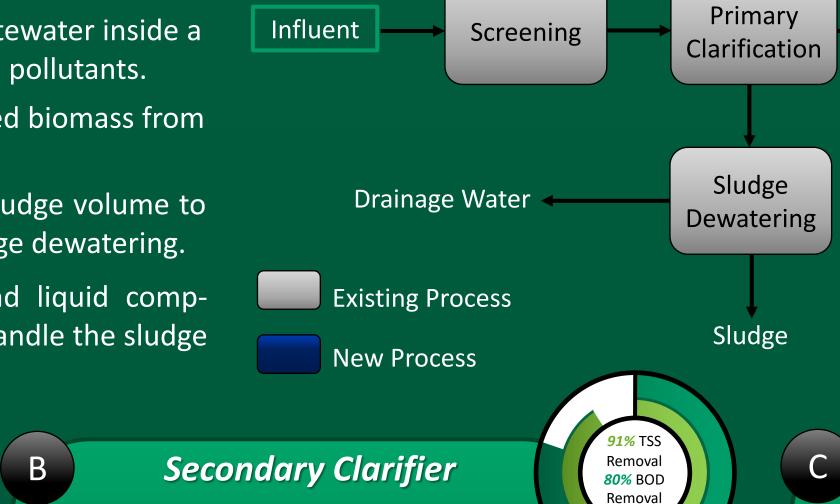




Moving Bed Biofilm Reactor

The carrier media increases the internal surface for optimal contact of water, air, and bacteria

The additional contact will allow high amount of soluble BOD removal in a compact space



The secondary clarifier will be in a

which will leave space for

future upgrades

Aluminum Sulfate

ate the small solids

handling

will be used to floccul-

Settled sludge is skimmed

by the hopper to sludge

rectangular shape for its compact design

L: 84m

W: 24m

Defoamer,

Caustic soda &

Nutrient

C Spiral De-waterer The spiral de-waterer is used to thicken the secondary sludge prior to intensive sludge dewatering

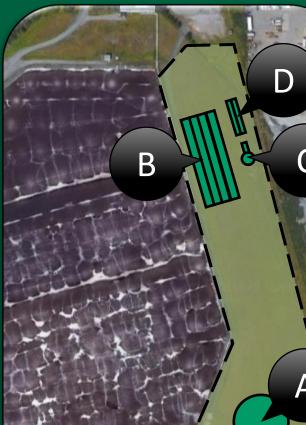
Packed

Aeration

► Entering sludge will settle in the lower pool area, then get pushed using a slowmoving screw Slurry will be

thickened by drainage in the up-L: 8.5m per part of the screw W: 4.0m



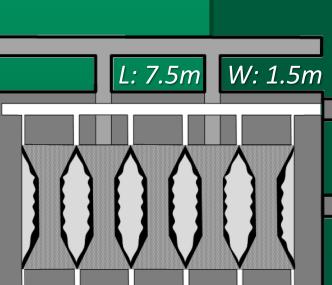






Expandable plates use compressed air to further remove water

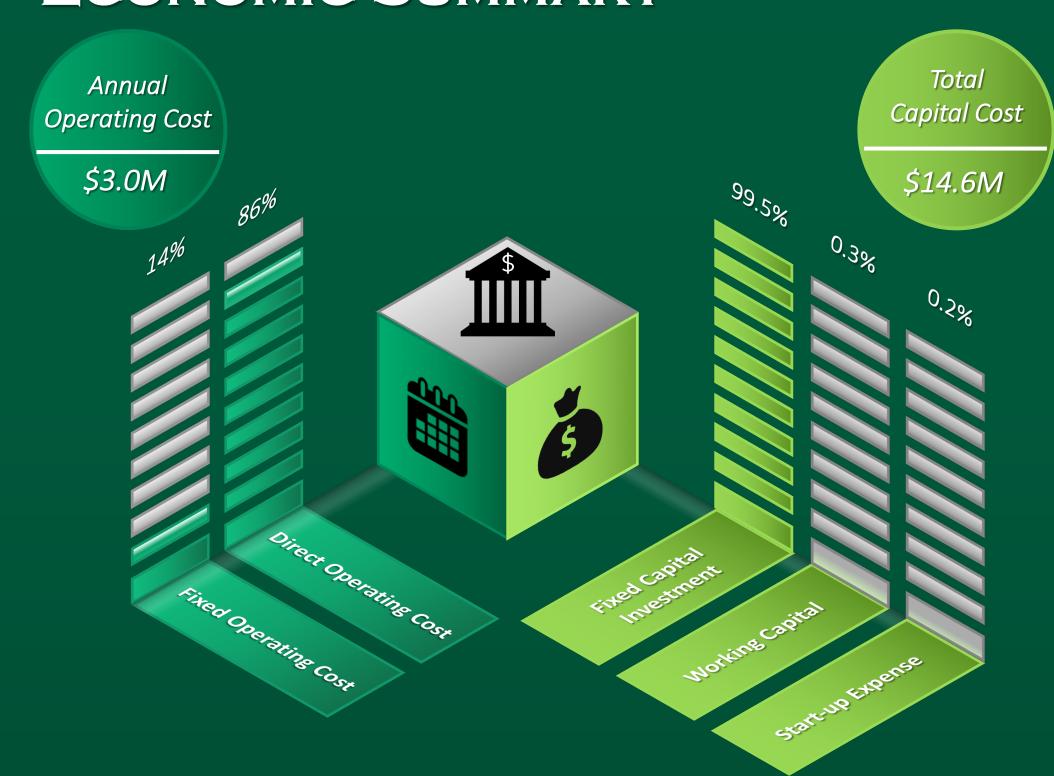
The sludge cakes will be trucked to farms to be used as a source of nutrients



Increase from

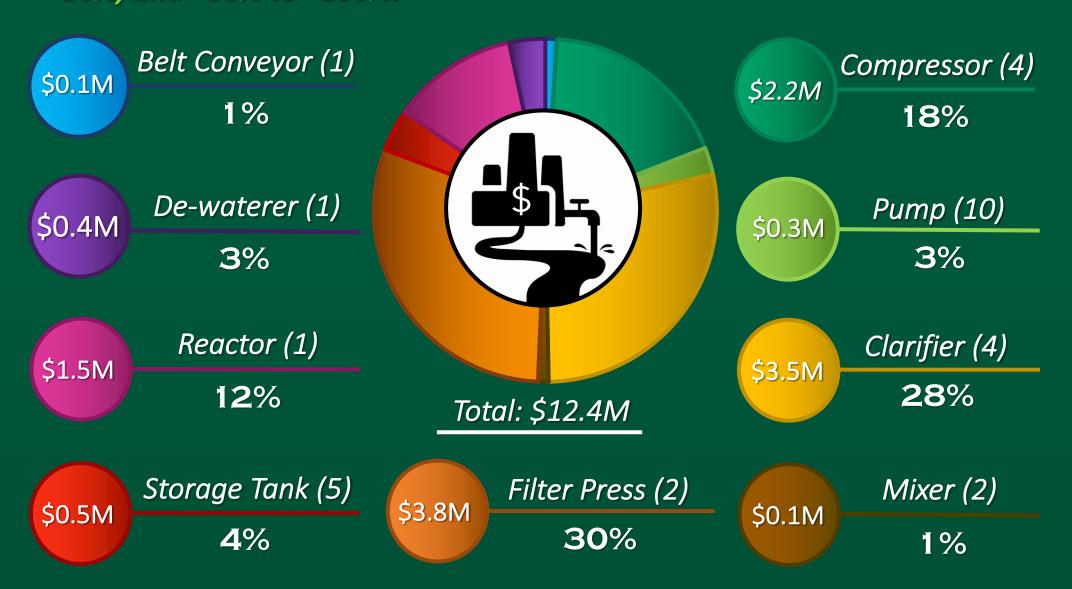
5% to **20%**

ECONOMIC SUMMARY

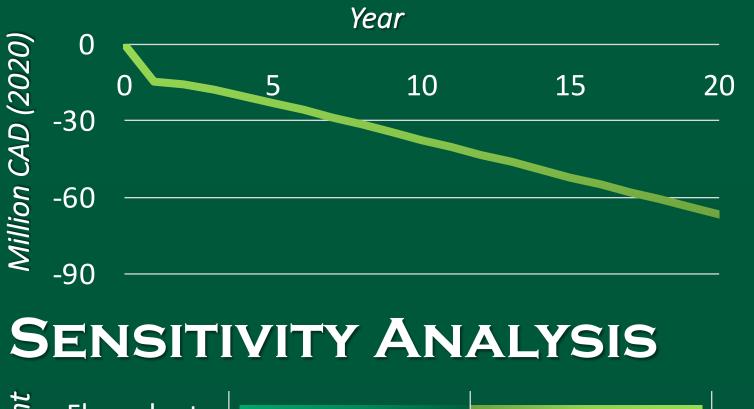


BARE MODULE EQUIPMENT COST

This feasibility study was completed as a *Class 5 estimate*. This means the accuracy of the costs within this analysis can vary between -20% to -50%, and +30% to +100%.



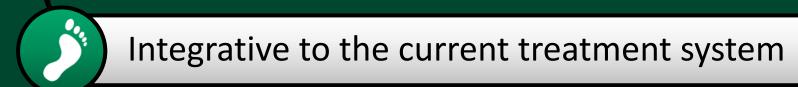
NET CASH FLOW

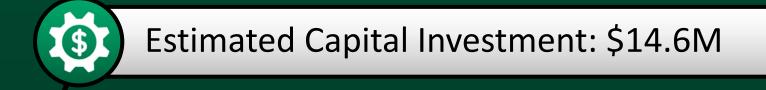


Flocculant Filter Press Clarifier MBBR De-waterer -3.00% 0.00% 3.00% Change in Cost of Treatment per Cubic Meter

KEY TAKEAWAYS

Exceeds required BOD and TSS reduction





Estimated Annual Operating Cost: \$3.0M

CONCLUSIONS

The upgrade produces effluent that will beat the newly proposed discharge limits. Process technologies were chosen using decision matrices, where 20 technologies were investigated. Using this selection process, the MBBR was added to supplement the removal of the high-loading soluble BOD. The generation of TSS through biological treatment required the addition of a secondary clarifier, and sludge dewatering system. The process has minimized environmental impact by increasing removal of total BOD and TSS from 90% and 60% to 98% and 95% respectively. This upgrade enables Irving Paper mill to continue day-to-day operations while minimizing environmental loading by producing effluent that meets the proposed regulation for TSS discharge, while being 20% lower for BOD, all in the worst case.

RECOMMENDATIONS

- ▶ It is recommended that IPL move forward to a detailed design phase. This process can exceed the newly proposed Pulp and Paper Effluent Regulations and has feasible avenues for improvement and optimization.
- ▶ Prepare an excess of carrier media as this design uses a MBBR carrier fill of 50% total volume,
- where it may be filled to 70%, providing more BOD removal for future stringent regulations. Lab testing for the optimal addition of flocculant prior to the clarification system allows for increased solids removal, providing saving to solids handling fees.



UNIVERSITY OF NEW BRUNSWICK



We would like to thank Irving

Paper Limited and the following

individuals for their support



